

TABLE 13.25 (continued)

Cu Ft Free Air Per Min	Nominal Diameter, In.											
	½	¾	1	1¼	1½	1¾	2	2½	3	3½	4	4½
1,500	76.1	39.0	21.3
1,600	86.6	44.3	24.2
1,700	97.8	50.1	27.4
1,800	110	56.1	30.7
1,900	122	62.7	34.2
2,000	135	69.3	37.9
2,100	149	76.4	40.8
2,200	166	83.6	45.8
2,300	179	91.6	50.1
2,400	195	99.8	54.6
2,500	212	108.2	59.2
2,600	229	117.2	64.0
2,700	247	126	69.1
2,800	265	136	74.3
2,900	285	146	79.8
3,000	305	156	85.2
3,200	347	177	97.1
3,400	391	200	109.5
3,600	438	224	122.8
3,800	488	250	137
4,000	542	277	151
4,200	605	305	168
4,400	668	335	183
4,600	736	366	200
4,800	809	399	218
5,000	883	433	236
5,250	967	477	260

5,500	524	286	158
5,750	605	313	173
6,000	690	341	188
6,500	809	402	222
7,000	944	464	256
7,500	1094	532	294
8,000	1259	615	335
9,000	1542	732	423
10,000	1865	876	523
11,000	2229	1044	636
12,000	2644	1236	764
13,000	3120	1454	918
14,000	3658	1704	1098
15,000	4269	1994	1314
16,000	4954	2324	1568
18,000	6054	2844	1944
20,000	7369	3444	2364
22,000	8904	4144	2844
24,000	10694	4944	3394
26,000	12744	5844	4044
28,000	15094	6944	4844
30,000	17744	8244	5844

* To determine the pressure drop in psi, the factor listed in the table for a given capacity and pipe diameter should be divided by the ratio of compression (from free air) at entrance of pipe, multiplied by the actual length of the pipe in feet, and divided by 1000.

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4,200	605	305	168
4,400	668	335	183
4,600	736	366	200
4,800	809	399	218
5,000	888	433	236
5,250	977	477	260

5,500	524	286	158	59.4	13.9	4.2	1.6
5,750	613	313	173	64.9	15.2	4.6	1.8
6,000	702	341	188	70.7	16.5	5.0	1.9
6,500	842	402	222	82.9	19.8	5.9	2.3
7,000	992	464	256	96.2	22.5	6.8	2.6
7,500	1152	532	294	110.5	25.8	7.8	3.0
8,000	1322	613	335	125.7	29.4	8.8	3.6
9,000	1602	722	423	159	37.2	10.2	4.4
10,000	1902	842	523	196	45.9	13.8	5.4
11,000	2232	972	613	237	55.5	16.7	6.5
12,000	2592	1112	702	282	66.1	19.8	7.7
13,000	3002	1262	802	332	77.5	23.3	9.0
14,000	3452	1422	902	387	89.9	27.0	10.5
15,000	3952	1592	1012	442	103.2	31.0	12.0
16,000	4502	1772	1112	503	117.7	35.3	13.7
18,000	5302	2082	1282	636	148.7	44.6	17.4
20,000	6202	2422	1482	755	174.7	55.0	21.4
22,000	7202	2802	1722	884	204.7	66.9	26.0
24,000	8302	3222	1982	1024	240.7	79.3	30.1
26,000	9502	3682	2282	1174	274.7	93.3	36.3
28,000	10802	4182	2642	1344	314.7	108.0	42.1
30,000	12202	4722	3022	1544	360.7	123.9	48.2

* To determine the pressure drop in psi, the factor listed in the table for a given capacity and pipe diameter should be divided by the ratio of compression (from free air) at entrance of pipe, multiplied by the actual length of the pipe in feet, and divided by 1000.

low oil pressure or excessive vibration, demand immediate shutdown. Protective control systems employing shutdown without indication, which merely drops out the holding coil of the motor starter, are usually warranted only on very small compressors.

Fail-safe circuitry is generally desirable. That is, added security is gained when a protective circuit must remain energized for normal compressor operation. A broken wire or burned-out component is guarded against automatically in this type of design.

A hand-reset sensing device or relay circuit that locks in the fault indication can be employed. This feature makes the protective system a troubleshooting aid.

To insure repeatability in sensing device set points, the sensing devices should be selected with positive adjustment features and should not be susceptible to vibration.

COMPRESSED-AIR DISTRIBUTION SYSTEM

Any drop in pressure between the compressor and the point of use is an unrecoverable loss. The distribution system is therefore one of the most important elements of the compressed air plant. In planning it, the following general rules should be observed:

1. Pipe sizes should be large enough that the pressure drop between the receiver and the point of use will not exceed 10 per cent of the initial pressure. Fittings offering least resistance to flow, such as long-radius elbows, should be selected. Provision should be made not only for present requirements but also for reasonable future growth.
2. Where it is possible, a loop system around the plant and within each shop and building is recommended. This gives a two-way distribution to the point where air demand is greatest. The loop pipe should be made large enough that the pressure drop will not be excessive at any outlet regardless of the direction of flow around the loop.
3. Long distribution lines, including those in a loop system, should have receivers of liberal size located near the far ends or at points of occasional heavy use. Many peak demands for air are of short duration, and storage capacity near such points avoids excessive pressure drop and may permit the use of a smaller compressor. Certain applications such as starting diesel engines or gas turbines are examples of this type of demand where the required rate may exceed the total compressor capacity.
4. Each header or main should be provided with outlets as close as possible to the point of application. This permits the use of the shorter hose lengths and avoids large pressure drops through the hose. Outlets should always be taken from the top of the pipe line to prevent carryover of condensed moisture to tools.
5. All piping should be sloped so that it drains toward a drop leg or moisture trap in order that condensation may be removed to prevent its reaching air-operated devices in which it would be harmful. The slope of the lines should always be

away from the compressor to prevent flow back into the compressor cylinder. A slope of about 1/4 in./ft (2.0 mm/m) may be used, with drains provided at all low points. These may consist of a short pipe with a trap or drain at the bottom.

6. For a system using only oil-free compressors, it is strongly recommended that corrosion-resistant pipe be used. Unlike a system using lubricated compressors in which an oil film will form to protect the pipe from the corrosive effect of the moisture in the warm air, a nonlubricated system will experience corrosion. This corrosion can lead to contamination of products and control systems.

Distribution Piping

Pipe size may be taken from Tables 13.21 to 13.26 once the air requirement is known. Such a determination is shown in the following example. For design purposes, pressure drop in a main line may be taken at 3 psig (0.20 bar) or less.

Example

Determination of pipe size for the plant air-distribution system (see Fig. 4.8). Compressor pressure is 105 psig (7.2 bars). The main air line to the cleaning room is 100 ft (30.5 m) long.

Step 1. *Air flow:* The tabulated requirement of the cleaning room is 332 cfm (564 cmh) of free air. Allowing 10 per cent for leakage and 135 ft³ (229 cmh) for additions, the requirement is 500 cfm (849.5 cmh).

Step 2. *Fittings:* Referring to Table 13.26 and assuming a 2-in. pipe (which may prove later to be incorrect), the length of straight pipe equivalent to the fittings is as follows:

One elbow at 5.17 ft	5.17 ft (1.58 m)
Two tees, reducing, at 5.17 ft	10.34 ft (3.16 m)
Two crosses, taken same as tees, at 5.17 ft	10.34 ft (3.16 m)
Total for fitting	25.85 ft (7.89 m)
Total equivalent length	125.85 ft (38.36 m)

Step 3. *Allowable pressure drop:* Pressure drop for entire line should not exceed 3 psig (0.20 bar). For part of line leading to cleaning room, allow 1 psig (0.07 bar).

Step 4. *Predicted pressure drop:* For the assumed 2-in. pipe and opposite 500 cfm, Table 13.26 gives a pressure drop of 19.2 psig per 1000-ft length. Thus, the pressure drop is

$$\frac{125.85 \text{ ft (38.4 m)}}{1000} \times 19.2 = 2.40 \text{ psig (0.166 bar)}$$

which when added to the 1 psig (0.070 bar) allowed for the room line is excessive.